

## A NOTE ON DISSIPATION IN FREE-CONVECTION

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### NOMENCLATURE

$c_p$ ,	specific heat at constant pressure;
$x, y$ ,	distances along and perpendicular to the plate;
$u, v$ ,	velocity components along $x$ and $y$ directions;
$Gr_\infty$	local Grashof number defined by (2);
$g$ ,	acceleration due to gravity;
$k$ ,	thermal conductivity;
$t$ ,	temperature;
$f$ ,	non-dimensional stream-function;
$F$ ,	transformed stream-function in the inner layer;
$G$ ,	transformed stream-function in the outer layer;
$T$ ,	function of $x$ defined by (2);
$q''$ ,	rate of heat-flux at the surface.

### Greek symbols

$\gamma$ ,	a constant;
$\psi$ ,	stream-function;
$\sigma$ ,	Prandtl number;
$\epsilon$ ,	local dissipation number defined by (2);
$\beta$ ,	co-efficient of volume expansion of the fluid;
$\eta$ ,	similarity variable defined by (2);
$\nu$ ,	kinematic viscosity;
$\alpha$ ,	thermal diffusivity;
$\theta$ ,	temperature excess;
$\phi$ ,	non-dimensional temperature function defined by (2);
$\zeta$ ,	stretched similarity variable;
$\Phi$ ,	transformed temperature function.

### Subscripts

$w$ ,	wall condition;
$\infty$ ,	condition at large distance from the plate;
$0$ ,	no dissipation;
$1$ ,	first order dissipation effects.

### INTRODUCTION

GEBHART [1] investigated effects of viscous dissipation in natural convection about semi-infinite flat vertical surfaces subject to both isothermal and uniform heat-flux surface conditions. He used a perturbation method and calculated the first temperature perturbation function for the Prandtl numbers ( $\sigma$ )  $10^{-2}$ ,  $0.72$ ,  $10^2$  and  $10^4$  for the former case and

for  $10^2$  for the latter. For the isothermal case, he put forward a conjecture regarding the asymptotic behaviour of the first temperature perturbation function as  $\sigma \rightarrow \infty$ . Roy [2], using the double-boundary-layer concept first introduced by Stewartson and Jones [3], obtained solutions for isothermal surfaces in powers of  $\sigma$ , for large  $\sigma$ , to terms  $O(\sigma^{-1/2})$ , and substantiated the above-mentioned conjecture.

In this paper, we propose to solve the high Prandtl number problem for uniform heat-flux surface conditions using a similar technique. The solutions will be obtained to terms  $O(\sigma^{-1})$ . It will be seen that there still exists an asymptotic behaviour of the first temperature perturbation function.

### ANALYSIS

The well-known equations for conservation of mass, momentum and energy are

$$\left. \begin{aligned} \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} &= 0, \\ u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} &= \nu \frac{\partial^2 u}{\partial y^2} \pm g\beta\theta, \\ u \frac{\partial \theta}{\partial x} + v \frac{\partial \theta}{\partial y} &= \alpha \frac{\partial^2 \theta}{\partial y^2} + \frac{\nu}{c_p} \left( \frac{\partial u}{\partial y} \right)^2, \end{aligned} \right\} \quad (1)$$

subject to the boundary conditions

$$\begin{aligned} u = v = 0, \quad q'' &= -k \frac{\partial \theta}{\partial y}, \quad y = 0, \\ u \rightarrow 0, \quad \theta \rightarrow 0 \quad &\text{as } y \rightarrow \infty. \end{aligned}$$

In the above,  $u, v$  are the velocity components,  $\theta$  is the temperature excess ( $t - t_\infty$ ),  $x$  is measured from the leading edge along the plate and  $y$  is the distance out perpendicular to the plate,  $q''$  is the rate of heat-flux at the surface, the plus and minus signs apply for heating and for cooling of the fluid respectively and the other symbols have their usual meanings.

Perturbation-type similar solutions of (1) are given by

$$\left. \begin{aligned} u &= \frac{\partial \psi}{\partial y}, & v &= -\frac{\partial \psi}{\partial x}, \\ \phi &= T(t_\infty - t) = \phi_0 \pm 5\epsilon\phi_1 \pm \dots, \\ \psi &= \nu 5^{\frac{1}{2}}(Gr_x)^{\frac{1}{2}}(f_0 \pm 5\epsilon f_1 + \dots), \\ Gr_x &= \left| \frac{g\beta x^4 q''}{kv^2} \right|, \\ \eta &= \frac{y}{x} \left( \frac{Gr_x}{5} \right)^{\frac{1}{2}}, \\ \epsilon &= \frac{g\beta x}{c_p}, \\ T(x) &= \frac{k}{xq''} \left( \frac{Gr_x}{5} \right)^{\frac{1}{2}}, \end{aligned} \right\} \quad (2)$$

where  $f$ 's and  $\phi$ 's are functions of  $\eta$  alone. We further assume, with Gebhart, that  $f_1 = 0$ . Thus the equations to be satisfied by  $f_0$ ,  $\phi_0$  and  $\phi_1$  are

$$f_0''' + 4f_0 f_0'' - 3(f_0')^2 - \phi_0 = 0, \quad (3)$$

$$\phi_0'' + \sigma(4f_0 \phi_0' - f_0' \phi_0) = 0, \quad (4)$$

$$\phi_1'' + \sigma(4f_0 \phi_1' - 6f_0' \phi_1 - f_0''^2) = 0, \quad (5)$$

together with the boundary conditions

$$\left. \begin{aligned} f_0(0) &= f_0'(0) = f_0'(\infty) = \phi_0(0) = 1 = \\ \phi_0(\infty) &= \phi_1(0) = \phi_1(\infty) = 0. \end{aligned} \right\} \quad (6)$$

It should be noted that what appears as  $\phi$  in Gebhart [1] is  $-\phi$  in our notations, in line with Sparrow and Gregg [4] who solved the no-dissipation problem for discrete values of  $\sigma$ .

### INNER AND OUTER LAYERS

For large values of  $\sigma$ , the effects of temperature variation are confined to a very thin layer lying well within the velocity boundary layer. In the case of isothermal surfaces, their thicknesses are 0 ( $\sigma^{-\frac{1}{2}}$ ) and 0 ( $\sigma^{\frac{1}{2}}$ ) respectively [2, 3]. However, in the present case these are 0 ( $\sigma^{-\frac{1}{2}}$ ) and 0 ( $\sigma^{\frac{3}{10}}$ ), their ratio remaining  $\sigma^{-\frac{1}{2}}$  as in the former case. The appropriate transformations are:

*Inner layer*

$$\left. \begin{aligned} \zeta_1 &= \sigma^{\frac{1}{2}} \eta, \\ f_0 &= \sigma^{-\frac{1}{2}} F_0(\zeta_1), \\ \phi_0 &= \sigma^{-\frac{1}{2}} \Phi_0(\zeta_1), \\ \phi_1 &= \sigma^{-\frac{1}{2}} \Phi_1(\zeta_1); \end{aligned} \right\} \quad (7)$$

*Outer layer*

$$\left. \begin{aligned} \zeta_2 &= \gamma \sigma^{-\frac{3}{10}} \eta, \\ f_0 &= \gamma \sigma^{-\frac{3}{10}} G_0(\zeta_2), \\ \phi_0 &= \phi_1 = 0; \end{aligned} \right\} \quad (8)$$

where  $\gamma$  is a suitable constant to be specified later. The corresponding equations for  $F_0$ ,  $\Phi_0$ ,  $\Phi_1$  and  $G_0$  are

$$F_0''' - \Phi_0 + \sigma^{-1} \{4F_0 F_0'' - 3(F_0')^2\} = 0, \quad (9)$$

$$\Phi_0'' + 4F_0 \Phi_0' - F_0' \Phi_0 = 0, \quad (10)$$

$$\Phi_1'' + 4F_0 \Phi_1' - 6F_0' \Phi_1 - (F_0'')^2 = 0, \quad (11)$$

$$G_0''' + 4G_0 G_0'' - 3(G_0')^2 = 0. \quad (12)$$

In the above, a prime denotes differentiation with respect to the appropriate variable,  $\zeta_1$  or  $\zeta_2$ . The boundary conditions at  $\eta = \infty$  are redundant for  $F_0$ , and those at  $\eta = 0$  for  $G_0$ . Further, equations (9)–(12) suggest that series solutions in some negative powers of  $\sigma$  exist. The appropriate series and the boundary conditions at  $\zeta_1 = \infty$  and at  $\zeta_2 = 0$  are determined by matching the inner solutions for large values of  $\zeta_1$  with the outer solutions for small values of  $\zeta_2$ . They are

$$\left. \begin{aligned} F_0 &= \sum_{i=0}^{\infty} \sigma^{-i/2} F_{0i}, \\ \Phi_0 &= \sum_{i=0}^{\infty} \sigma^{-i/2} \Phi_{0i}, \\ \Phi_1 &= \sum_{i=0}^{\infty} \sigma^{-i/2} \Phi_{1i}, \\ G_0 &= \sum_{i=0}^{\infty} \sigma^{-i/2} G_{0i}; \end{aligned} \right\} \quad (13)$$

and

$$F_{00}'(\infty) = 0,$$

$$F_{01}'(\infty) = \gamma^3 G_{00}'(0),$$

$$F_{02}'(\infty) = \lim_{\zeta_1 \rightarrow \infty} \gamma^3 \{G_{01}'(0) + 3\gamma \zeta_1\},$$

$$G_{00}(0) = 0,$$

$$G_{00}'(0) = 1, \quad \text{choosing } \gamma^2 = \lim_{\zeta_1 \rightarrow \infty} F_{00}'(\zeta_1)$$

$$G_{01}(0) = \lim_{\zeta_1 \rightarrow \infty} \{1/\gamma F_{00}(\zeta_1) - \gamma \zeta_1\},$$

$$G_{01}'(0) = \lim_{\zeta_1 \rightarrow \infty} \{1/\gamma^2 F_{01}'(\zeta_1) - \gamma \zeta_1 G_{00}'(0)\},$$

$$G_{02}(0) = \lim_{\zeta_1 \rightarrow \infty} \{1/\gamma F_{01}(\zeta_1) - \gamma \zeta_1 G_{01}(0) - \gamma^2/2 \zeta_1^2 G_{00}'(0)\},$$

$$G_{02}'(0) = \lim_{\zeta_1 \rightarrow \infty} \{1/\gamma^2 F_{02}'(\zeta_1) - \gamma \zeta_1 G_{01}'(0) - 3/2 \gamma^2 \zeta_1^2\}.$$

### SOLUTIONS

The twelve equations that are obtained from (9)–(13) have been solved on the computer. The unknown boundary conditions required to start numerical integrations are given below:

$$F_{00}'(0) = 0.811546, \quad \Phi_{00}(0) = -1.147565,$$

$$\begin{aligned}
F''_{01}(0) &= -0.173879, & \Phi_{01}(0) &= -0.226844, \\
F''_{02}(0) &= 0.134655, & \Phi_{02}(0) &= 0.030392, \\
G_{00}(0) &= 0.0, & G'_{00}(0) &= 1, & G''_{00}(0) &= -1.837319, \\
G_{01}(0) &= -0.300701, & G'_{01}(0) &= 0.732916, \\
G'_{01}(0) &= -1.399446, & G_{02}(0) &= -0.311263, \\
G'_{02}(0) &= 0.804204, & G''_{02}(0) &= -1.578787, \\
\Phi_{10}(0) &= -0.118237, & \Phi_{11}(0) &= 0.077670, \\
\Phi_{12}(0) &= -0.094576.
\end{aligned}$$

### CONCLUSIONS

The effect of viscous dissipation in the case of an assigned surface heat-flux is to make necessary a larger difference between  $t_w$  and  $t_\infty$  for the convection of a heat-flux to the fluid. The surface temperature is given by the relationship

$$t_w - t_\infty = - \frac{q'' x / k}{(\sigma Gr_x / 5)^{1/4}} \times [1.147565 + 0.226844\sigma^{-1/4} - 0.030392\sigma^{-1}] [1 + 5\epsilon],$$

where

$$r = \frac{\phi_1(0)}{\phi_0(0)} = 0.103033 - 0.088049\sigma^{-1/4} + 0.102548\sigma^{-1}.$$

The important ratio  $r$  has the values 0.085444, 0.095253, 0.100351 and 0.102163 for  $\sigma = 10, 10^2, 10^3$  and  $10^4$  respectively. The value given by Gebhart [1] for  $\sigma = 10^2$ , namely 0.09547, compares very well with the corresponding value obtained above. However, though  $r$  increases with  $\sigma$  it has an asymptotic value 0.103033 for  $\sigma = \infty$ .

### REFERENCES

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### NOTE ADDED IN PROOF

A more recent paper is B. Gebhart and J. Mollendorf, Viscous dissipation in external natural convection flows, *J. Fluid Mech.* **38**, 97–107 (1969).

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## PREDICTION OF FLOW AND HEAT TRANSFER IN TURBULENT CYLINDRICAL WALL JETS

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### NOMENCLATURE

$C$ , a curvature parameter ( $\equiv d/S$ );  
 $c_p$ , specific heat at constant pressure;  
 $d$ , diameter of the rod;  
 $h$ , local heat-transfer coefficient;

$K$ , a mixing-length constant;  
 $l$ , the mixing length;  
 $p$ , pressure;  
 $q$ , heat flux;  
 $r$ , distance from the axis of symmetry;  
 $r_i$ , radius of inner boundary of the wall jet (i.e. the radius of the rod);  
 $Re_S$ , a Reynolds number ( $\equiv \rho u_S S / \mu$ );  
 $S$ , slot height;

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